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# **Increased Oxygen Recovery from Sabatier Systems Using Plasma Pyrolysis Technology and Metal Hydride Separation**

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# Overview

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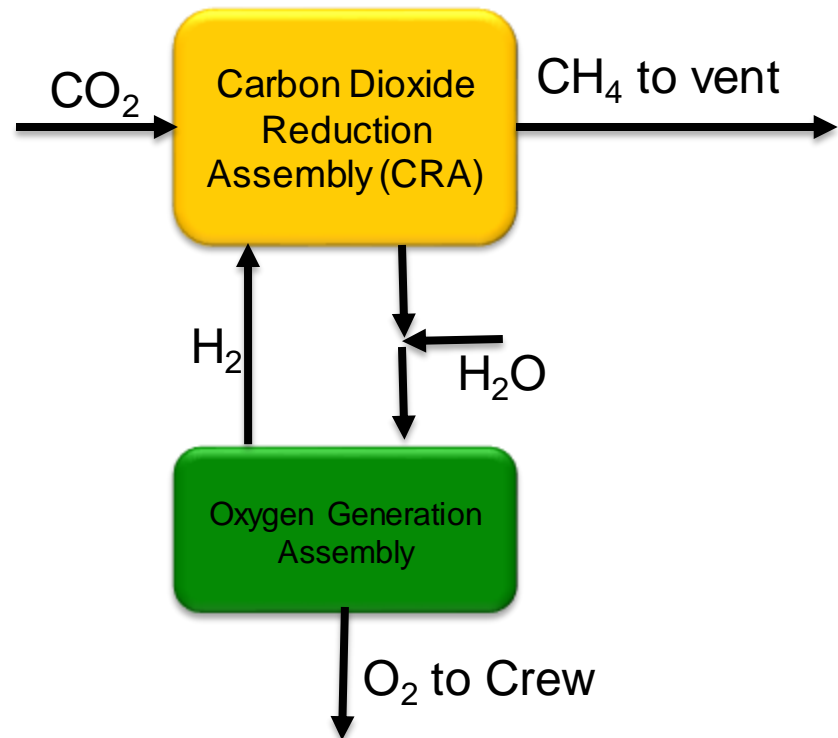
- Background
  - State-of-the-Art
  - Beyond State-of-the-Art
- PPA Technology Description
- Hydrogen purification
  - Metal Hydrides
- Objectives
- Method
- Results
- Conclusion
- Acknowledgements



# State-of-the-Art

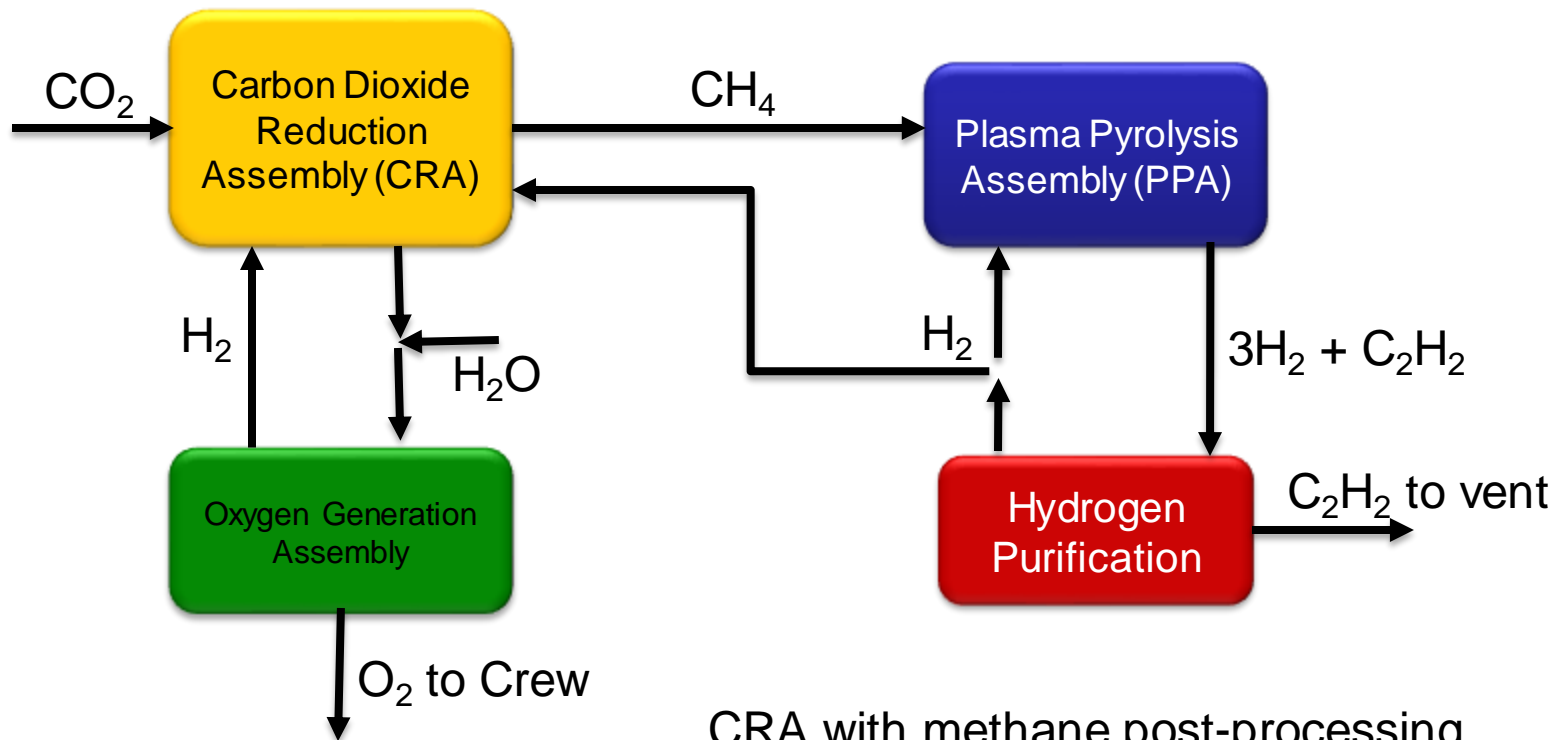
- Carbon Dioxide Reduction Assembly (CRA)= SOA ISS

- $\text{CO}_2 + 4\text{H}_2 \rightarrow 2\text{H}_2\text{O} + \text{CH}_4$
- Water product electrolyzed for oxygen
- Methane product vented resulting in loss of hydrogen reactant
- ~50% of  $\text{O}_2$  recovered from metabolic  $\text{CO}_2$





# Beyond State-of-the-Art



CRA with methane post-processing  
recovers 75-90% of O<sub>2</sub> from metabolic CO<sub>2</sub>



# PPA Technology Description

- Methane converted to hydrogen and acetylene by partial pyrolysis in microwave generated plasma
  - $2\text{CH}_4 \rightarrow 3\text{H}_2 + \text{C}_2\text{H}_2$
- First Generation UMPQUA Microwave Plasma Methane Pyrolysis Assembly (PPA) delivered in May 2009
- 3<sup>rd</sup> Gen. PPA, capable of 4CM flow rates, delivered October 2013



H<sub>2</sub>/CH<sub>4</sub> Plasma



3<sup>rd</sup> Gen PPA



# PPA Technology Description

- 3<sup>rd</sup> Gen. PPA integrated with Sabatier Development Unit (SDU) in Exploration Test Chamber
- PPA gets CH<sub>4</sub> from Sabatier Development Unit (SDU) or bottles
  - H<sub>2</sub> and CO<sub>2</sub> from bottles





# Hydrogen Purification

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- Primary methods of interest
  - Sorbents
    - SBIR in work
  - Solid polymer electrolysis
    - SBIR in work
  - Metal hydrides
    - MSFC preliminary investigation
- For use with  $C_2H_2$  must be below autoignition temp. ( $325^{\circ}C$ ) and exothermic decomposition pressure (200kPa)





# Metal Hydrides

- Form when  $H_2$  reacts with metal alloy to form chemical compound
  - $M + \frac{1}{2}xH_2 \leftrightarrow MH_x + \text{heat}$
- Reversible
  - La-Ni-Sn alloys present greatest cyclic durability and performance at PPA process conditions
- High volumetric packing density
  - Ex.  $LaNi_5H_{6.7}$  hydride has a volumetric density of  $7.6 \times 10^{22}$  atoms H/ml which is nearly 81% greater than the liquid  $H_2$  ( $4.2 \times 10^{22}$  atoms H/ml.)



Hydrogen Science & Technology Fact Sheet, Savannah River National Laboratory, 2009.





# Objectives

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- Evaluate performance of 3<sup>rd</sup> Gen. PPA
  - Stand-alone
  - Integrated with SDU
- Investigate metal hydride hydrogen purification



# Method: PPA Stand-Alone

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- Purpose: Verify performance consistent with UMPQUA's
- H<sub>2</sub> and CH<sub>4</sub> fed from ultra-high purity bottles
  - 4:1 ratio H<sub>2</sub>:CH<sub>4</sub>
- 1,2,3,4, and 5 crew member processing rates



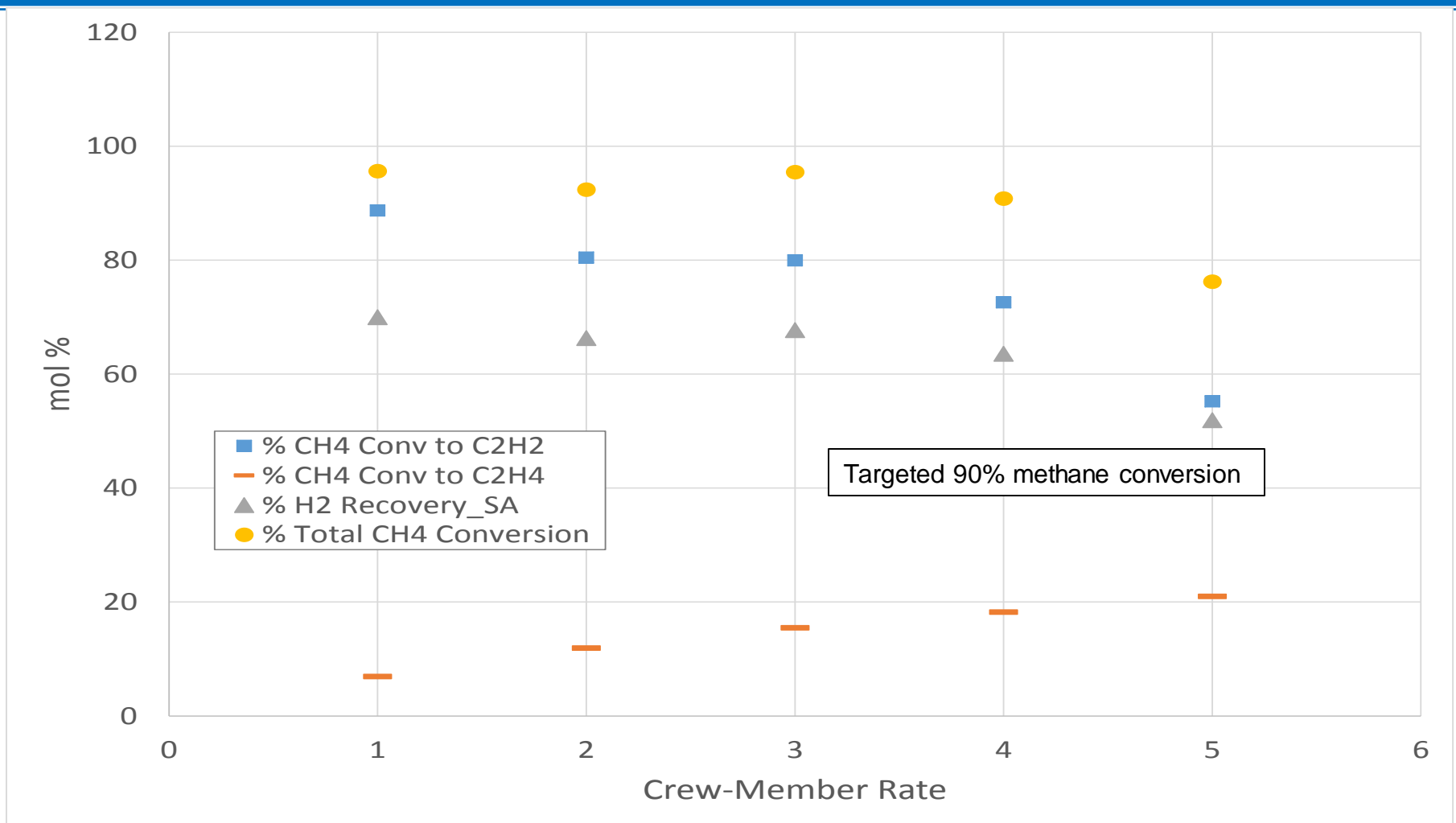
# Method: PPA Integrated

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- Purpose: Evaluate PPA performance with Sabatier Development Unit (SDU)  $\text{CH}_4$  feed stream
- SDU operated at  $\text{H}_2:\text{CO}_2$  ratio of 4.5:1
  - Ensured all  $\text{CO}_2$  was reacted
  - $\text{H}_2$  in SDU product
  - $\text{H}_2\text{O}$  in SDU product
- $\text{H}_2$  balance from bottles adjusted to maintain 4:1 ratio of  $\text{H}_2:\text{CH}_4$
- 2,3, and 4 crew member processing rates

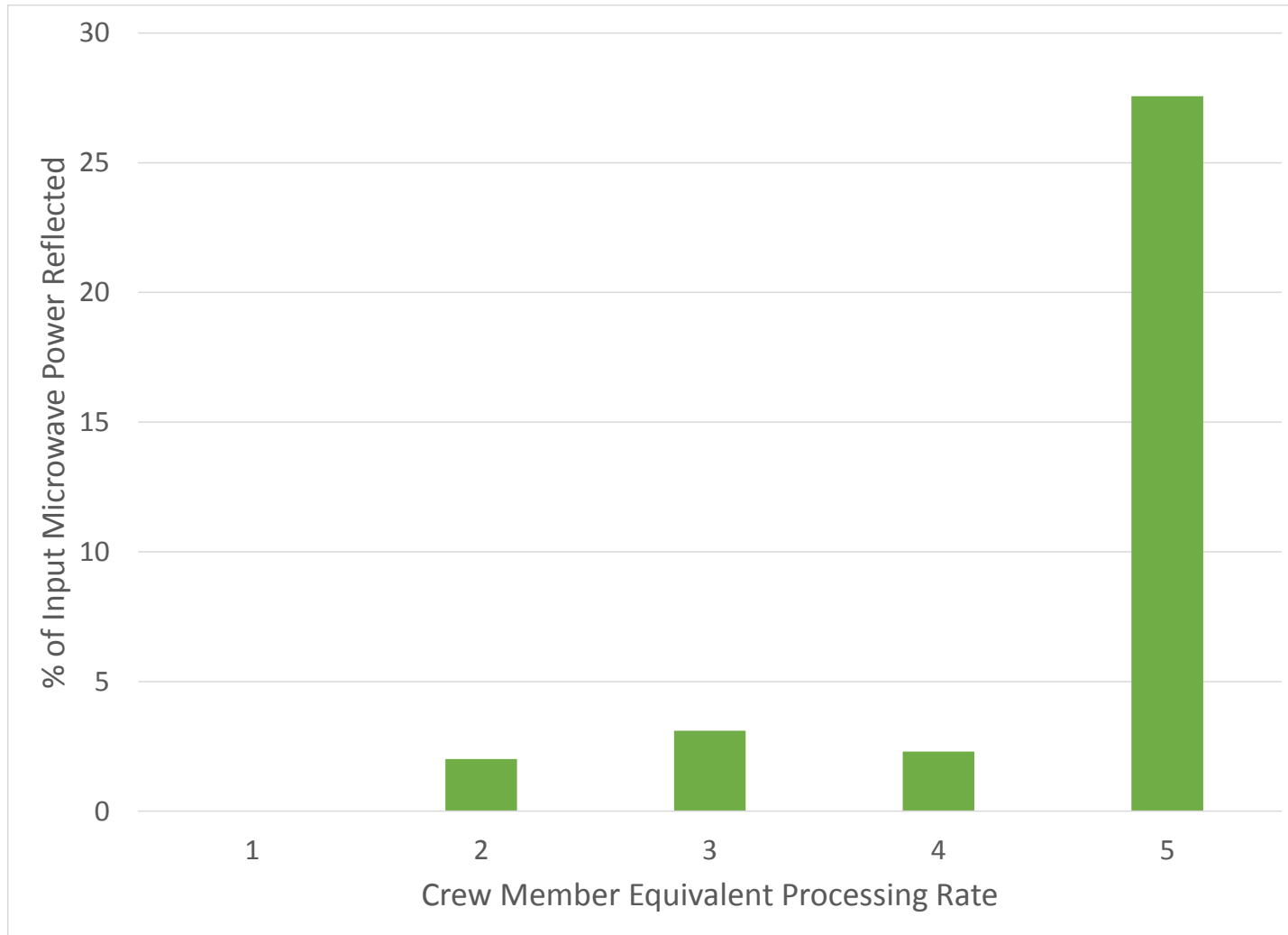


# Results: Stand-Alone



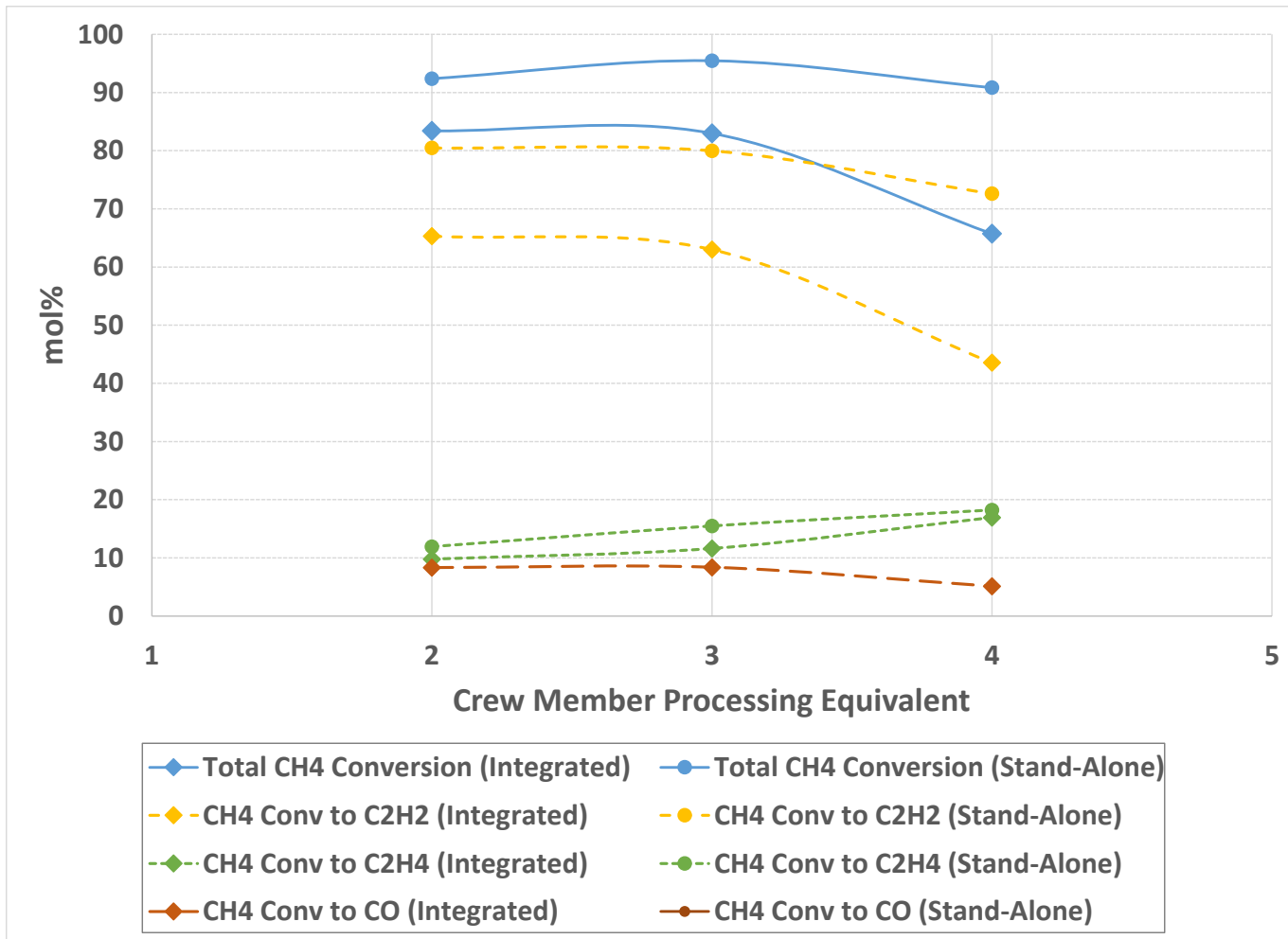


# Results: Stand-Alone



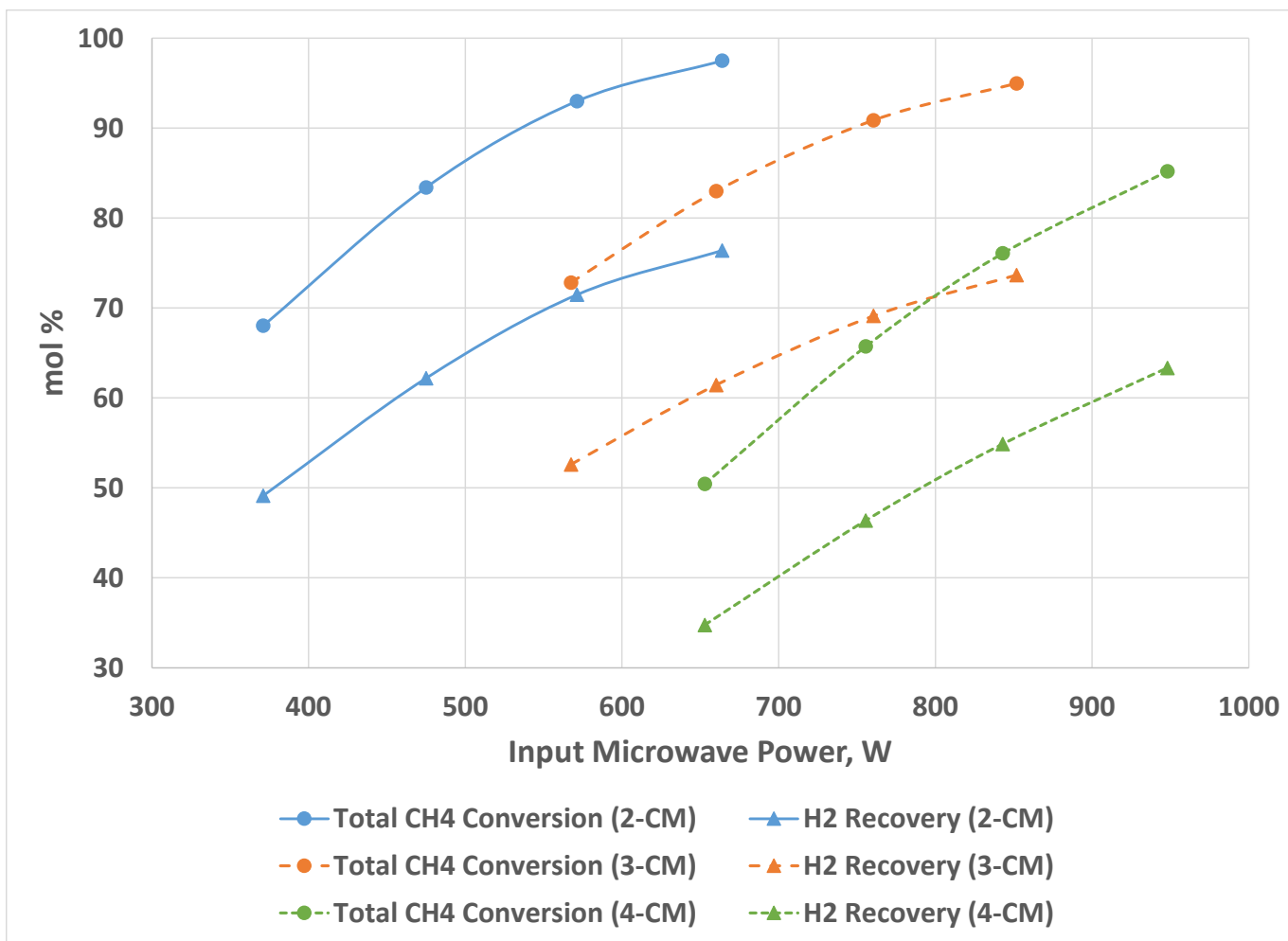


# Results: Stand Alone vs. Integrated





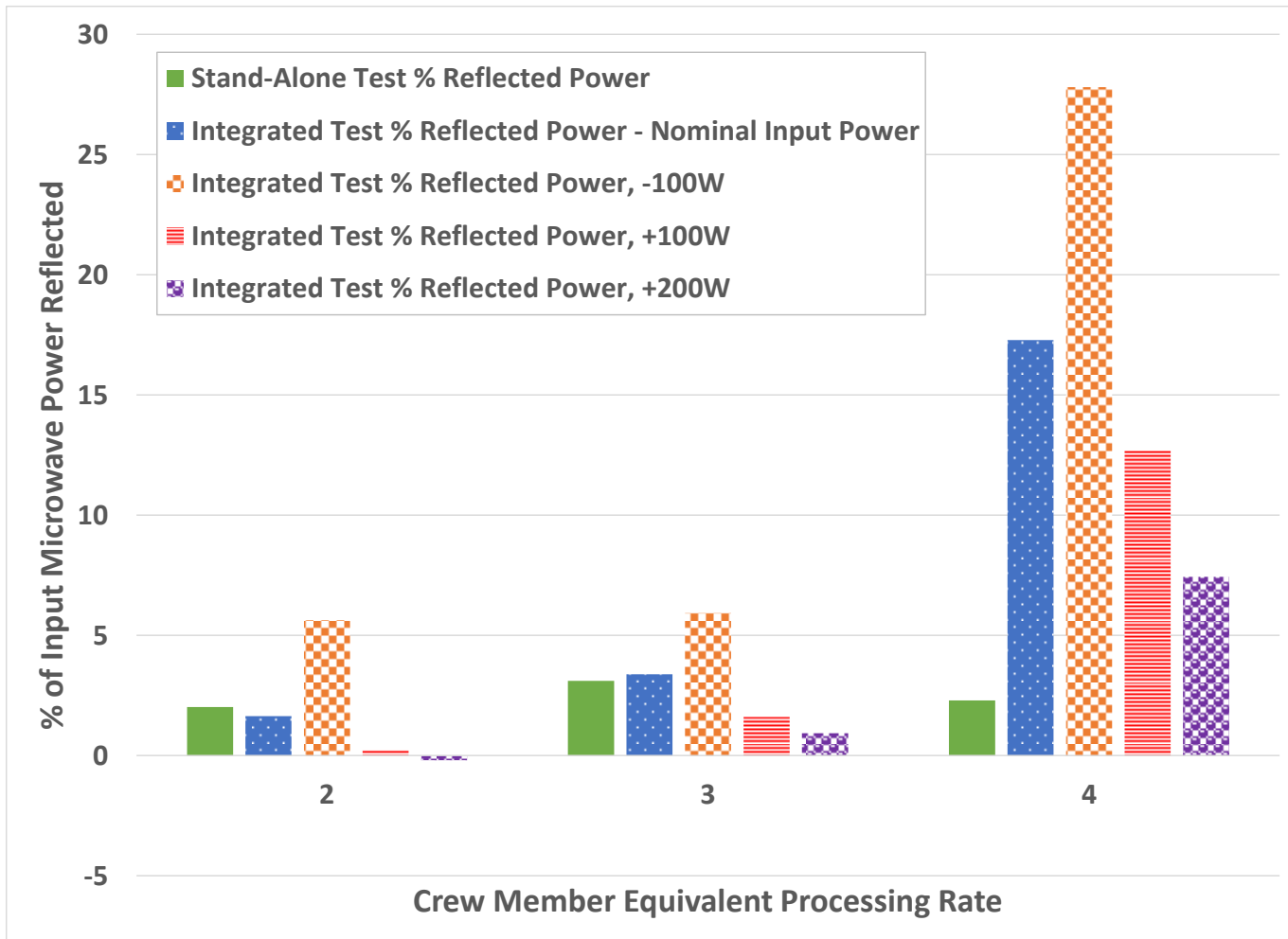
# Results: Integrated with SDU







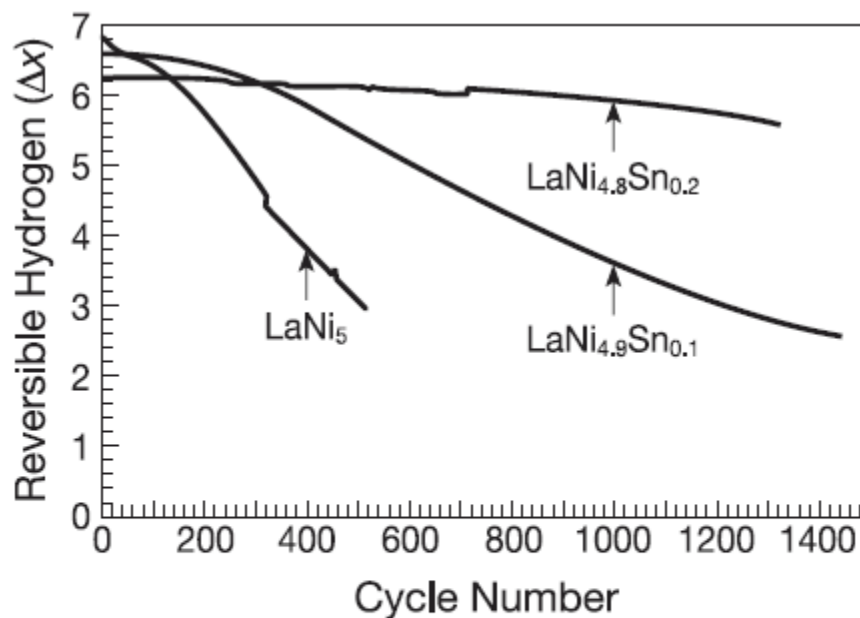
# Results: Integrated with SDU





# Results: Metal Hydrides

- $\text{LaNi}_{4.8}\text{Sn}_{0.2}$  alloy
  - >1.2 weight percent reversible hydrogen capacity
  - High cyclic durability
  - Adsorption-desorption pressure and temperature compatible with PPA process conditions
- 2.6 kg needed for one hour operation
- Three bed system mass ~10kg w/ 20% structure
- Absorption at 10 °C  
desorption at 25 °C



*Figure 2. Effect of Sn substitution on the reversible hydrogen-storage capacity of  $\text{LaNi}_{5-x}\text{Sn}_x$  hydrides after cycling between 295 K and 510 K.*

Bowman & Fultz, *Metal Hydrides I*, MRS Bulletin, 2002.



# Conclusion

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- PPA met targeted 90% CH<sub>4</sub> conversion in stand-alone operation
- Integrated operation showed less than targeted CH<sub>4</sub> conversion and H<sub>2</sub> recovery
  - Significant CO production resulted in decreased performance
  - Investigating performance improvements through microwave power adjustment and tuning
- Metal hydride separation system very viable for PPA application



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- Advanced Exploration Systems Advanced Resource Recovery and Environmental Monitoring
  - Jacobs Engineering
    - Tom Williams
    - Kenny Bodkin
    - Heath Mullins



# Questions?